

10-67 A cogeneration plant is to generate power and process heat. Part of the steam extracted from the turbine at a relatively high pressure is used for process heating. The net power produced and the utilization factor of the plant are to be determined.

Assumptions 1 Steady operating conditions exist. 2 Kinetic and potential energy changes are negligible.

Analysis From the steam tables (Tables A-4, A-5, and A-6),

$$h_1 = h_f @ 10 \text{ kPa} = 191.81 \text{ kJ/kg}$$

$$v_1 = v_f @ 10 \text{ kPa} = 0.00101 \text{ m}^3/\text{kg}$$

$$\begin{aligned} w_{p1,m} &= v_1(P_2 - P_1) \\ &= (0.00101 \text{ m}^3/\text{kg})(600 - 10 \text{ kPa}) \left(\frac{1 \text{ kJ}}{1 \text{ kPa} \cdot \text{m}^3} \right) \\ &= 0.60 \text{ kJ/kg} \end{aligned}$$

$$h_2 = h_1 + w_{p1,m} = 191.81 + 0.60 = 192.41 \text{ kJ/kg}$$

$$h_3 = h_f @ 0.6 \text{ MPa} = 670.38 \text{ kJ/kg}$$

Mixing chamber:

$$\dot{E}_{in} - \dot{E}_{out} = \Delta \dot{E}_{system} \overset{\text{no steady}}{\neq 0} \longrightarrow \dot{E}_{in} = \dot{E}_{out}$$

$$\sum \dot{m}_i h_i = \sum \dot{m}_e h_e \longrightarrow \dot{m}_4 h_4 = \dot{m}_2 h_2 + \dot{m}_3 h_3$$

$$\text{or, } h_4 = \frac{\dot{m}_2 h_2 + \dot{m}_3 h_3}{\dot{m}_4} = \frac{(22.50)(192.41) + (7.50)(670.38)}{30} = 311.90 \text{ kJ/kg}$$

$$v_4 = v_f @ h_4 = 311.90 \text{ kJ/kg} = 0.001026 \text{ m}^3/\text{kg}$$

$$\begin{aligned} w_{p2,m} &= v_4(P_5 - P_4) \\ &= (0.001026 \text{ m}^3/\text{kg})(7000 - 600 \text{ kPa}) \left(\frac{1 \text{ kJ}}{1 \text{ kPa} \cdot \text{m}^3} \right) \\ &= 6.57 \text{ kJ/kg} \end{aligned}$$

$$h_5 = h_4 + w_{p2,m} = 311.90 + 6.57 = 318.47 \text{ kJ/kg}$$

$$\left. \begin{array}{l} P_6 = 7 \text{ MPa} \\ T_6 = 500^\circ\text{C} \end{array} \right\} \begin{array}{l} h_6 = 3411.4 \text{ kJ/kg} \\ s_6 = 6.8000 \text{ kJ/kg} \cdot \text{K} \end{array}$$

$$\left. \begin{array}{l} P_7 = 0.6 \text{ MPa} \\ s_7 = s_6 \end{array} \right\} h_7 = 2774.6 \text{ kJ/kg}$$

$$\left. \begin{array}{l} P_8 = 10 \text{ kPa} \\ s_8 = s_6 \end{array} \right\} x_8 = \frac{s_8 - s_f}{s_{fg}} = \frac{6.8000 - 0.6492}{7.4996} = 0.8201$$

$$h_8 = h_f + x_8 h_{fg} = 191.81 + (0.8201)(2392.1) = 2153.6 \text{ kJ/kg}$$

Then,

$$\begin{aligned} \dot{W}_{T,out} &= \dot{m}_6(h_6 - h_7) + \dot{m}_8(h_7 - h_8) \\ &= (30 \text{ kg/s})(3411.4 - 2774.6) \text{ kJ/kg} + (22.5 \text{ kg/s})(2774.6 - 2153.6) \text{ kJ/kg} = 33,077 \text{ kW} \end{aligned}$$

$$\dot{W}_{p,m} = \dot{m}_2 w_{p1,m} + \dot{m}_4 w_{p2,m} = (22.5 \text{ kg/s})(0.60 \text{ kJ/kg}) + (30 \text{ kg/s})(6.57 \text{ kJ/kg}) = 210.6 \text{ kW}$$

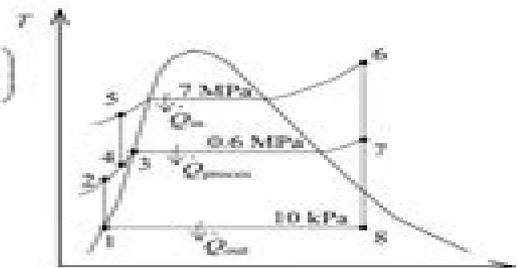
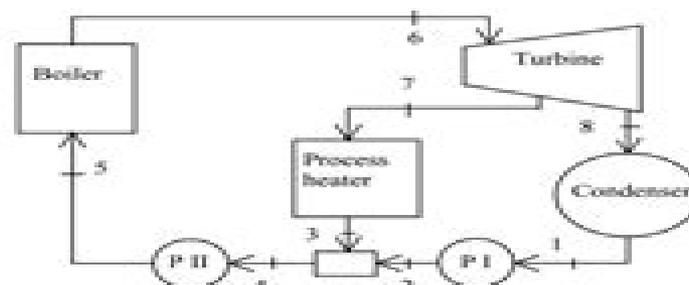
$$\dot{W}_{net} = \dot{W}_{T,out} - \dot{W}_{p,m} = 33,077 - 210.6 = \mathbf{32,866 \text{ kW}}$$

Also, $\dot{Q}_{process} = \dot{m}_7(h_7 - h_3) = (7.5 \text{ kg/s})(2774.6 - 670.38) \text{ kJ/kg} = 15,782 \text{ kW}$

$$\dot{Q}_{in} = \dot{m}_6(h_6 - h_5) = (30 \text{ kg/s})(3411.4 - 318.47) = 92,788 \text{ kW}$$

and

$$\eta_{th} = \frac{\dot{W}_{net} + \dot{Q}_{process}}{\dot{Q}_{in}} = \frac{32,866 + 15,782}{92,788} = \mathbf{52.4\%}$$



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