

to another unit. If the process fluid is not at the desired output temperature, the performance of the unit (reactor, etc.) may not be as good as desired, and therefore not as profitable.

1.1 The control block diagram for the process furnace is shown below in Figure 1. Where the the signals are



Figure 1-1: Control block diagram of process furnace follows:

- T_{set} : Temperature setpoint
- p_{in} : Valve top pressure
- F_{in} : Fuel gas flowrate
- F_p : Process fluid flowrate
- T_p : Process fluid inlet temperature
- T : Temperature of process fluid outlet
- T_m : Measured temperature

1.4

The problem statement tells us that the gasoline is worth \$200,000 a day. A 2% increase in value is:

$$\frac{\$200,000}{\text{day}} \times 0.02 = \frac{\$40,000}{\text{day}}$$

We are also given that the savings will cost \$2,000,000. We can now calculate the time required to payback the control system investment:

$$\frac{\$2,000,000}{\frac{\$40,000}{\text{day}}} = 200\text{days}$$

Therefore, we know it will take 200 days to pay off the investment.

1.7

$$2\text{yrs} = 4.4 \text{ million } \$/\text{yr} \times 0.25 = \$1,100,000$$

1.8

We know from the problem statement that the inlet (F_{in}) and outlet (F_{out}) flowrates can be represented with the following equations:

$$F_{in} = 50 + 10 \sin(0.1t)$$

$$F_{out} = 50$$

The change in volume as a function of time is

$$\frac{dV}{dt} = F_{in} - F_{out}$$

substituting what we know:

$$\frac{dV}{dt} = 50 + 10 \sin(0.1t) - 50$$

Simplifying

$$\frac{dV}{dt} = 10 \sin(0.1t)$$

Rearranging the equation

$$dV = 10 \sin(0.1t) dt$$

Taking the integral of both sides

$$\int dV = \int 10 \sin(0.1t) dt$$

Using basic calculus to solve

$$V - V_0 = \frac{-10}{0.1} \cos(0.1t) \Big|_{t=0}^t$$

We know the initial tank volume is 500 liters

$$V - 500 = -100 \cos(0.1t) - 100 \cos(0)$$

$$V - 500 = -100 \cos(0.1t) + 100$$

$$V(t) = 600 - 100 \cos(0.1t)$$

The equation above tells us how the volume of the tank will vary with time. This can also be seen visually in Figure 2 below.

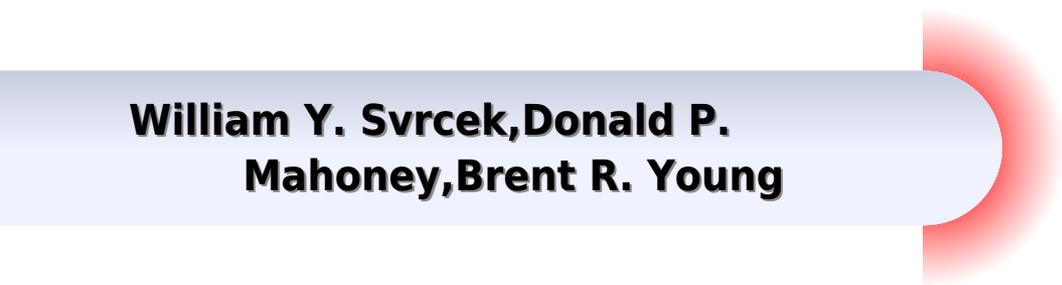
1.9

a.

The objective is to maintain a desired blood glucose concentration by insulin injection. Insulin is the manipulated input and blood glucose is the measured output. As performed by injections, the input is really discrete and not continuous. Also, glucose is not continuously measured, as the measured output is discrete. Disturbances include meal consumption and exercise. Feedforward action is used when a diabetic administers an injection to compensate for a

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Mahoney, Brent R. Young**



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Process Engineering Michael Kleiber, 2020-04-20 This book provides a comprehensive introduction to chemical process engineering linking the fundamental theory and concepts to the industrial practice This 2nd Edition contains new chapters on biological wastewater treatment dynamic simulation and PID discussion It enables the reader to integrate fundamental knowledge of the basic disciplines to understand key chemical processes and to apply this knowledge to the practice in industry

Perry's Chemical Engineers' Handbook, 9th Edition Don W. Green, Marylee Z. Southard, 2018-07-13 Up to Date Coverage of All Chemical Engineering Topics from the Fundamentals to the State of the Art Now in its 85th Anniversary Edition this industry standard resource has equipped generations of engineers and chemists with vital information data and insights Thoroughly revised to reflect the latest technological advances and processes Perry's Chemical Engineers Handbook Ninth Edition provides unsurpassed coverage of every aspect of chemical engineering You will get comprehensive details on chemical processes reactor modeling biological processes biochemical and membrane separation process and chemical plant safety and much more This fully updated edition covers Unit Conversion Factors and Symbols Physical and Chemical Data including Prediction and Correlation of Physical Properties Mathematics including Differential and Integral Calculus Statistics Optimization Thermodynamics Heat and Mass Transfer Fluid and Particle Dynamics Reaction Kinetics Process Control and Instrumentation Process Economics Transport and Storage of Fluids Heat Transfer Operations and Equipment Psychrometry Evaporative Cooling and Solids Drying Distillation Gas Absorption and Gas Liquid System Design Liquid Liquid Extraction Operations and Equipment Adsorption and Ion Exchange Gas Solid Operations and Equipment Liquid Solid Operations and Equipment Solid Solid Operations and Equipment Chemical Reactors Bio based Reactions and Processing Waste Management including Air Wastewater and Solid Waste Management Process Safety including Inherently Safer Design Energy Resources Conversion and Utilization Materials of Construction

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and analyzing multi loop control systems today industry practitioners employ both steady state and dynamic simulation based methodologies These real time methods have now all but replaced the traditional approach A Real Time Approach to Process Control provides the student with both a theoretical and practical introduction to this increasingly important approach Assuming no prior knowledge of the subject this text introduces all of the applied fundamentals of process control from instrumentation to process dynamics PID loops and tuning to distillation multi loop and plant wide control In addition students come away with a working knowledge of the three most popular dynamic simulation packages The text carefully balances theory and practice by offering students readings and lecture materials along with hands on workshops that provide a virtual process on which to experiment and from which to learn modern real time control strategy development Features The first and only textbook to use a completely real time approach Gives students the opportunity to understand and use HYSYS software Carefully designed workshops tutorials have been included to allow students to practice and apply the theory Includes many worked examples and student problems VISIT THE AUTHORS WEBSITE www.ench.ucalgary.ca/realtime **Process Dynamics and Control** American Institute of Chemical Engineers,1961 Process Dynamics and Control, 5th Edition Seborg,2017-10-17 **Process Dynamics, Modeling, and Control** Babatunde Ayodeji Ogunnaike,Willis Harmon Ray,1994 This text offers a modern view of process control in the context of today s technology It provides the standard material in a coherent presentation and uses a notation that is more consistent with the research literature in process control Topics that are unique include a unified approach to model representations process model formation and process identification multivariable control statistical quality control and model based control This book is designed to be used as an introductory text for undergraduate courses in process dynamics and control In addition to chemical engineering courses the text would also be suitable for such courses taught in mechanical nuclear industrial and metallurgical engineering departments The material is organized so that modern concepts are presented to the student but details of the most advanced material are left to later chapters The text material has been developed refined and classroom tested over the last 10 15 years at the University of Wisconsin and more recently at the University of Delaware As part of the course at Wisconsin a laboratory has been developed to allow the students hands on experience with measurement instruments real time computers and experimental process dynamics and control problems

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